

### **Amendments to the Specification**

Please replace the paragraph beginning at page 27, line 18 with the following amended paragraph:

An example of a production set up for the back pulse using permeate is shown in Fig. 4. During the primary filtration process, the suspension in retentate vessel 1 located on means for maintaining constant weight 2 such as a scale or load cell, is recirculated through cross flow module(s) 3. These modules can be of any configuration if the manufacturer recommends the possibility of reverse pressurization of the membrane. Recirculation is achieved using retentate pump 4 of a peristaltic pump type or positive displacement pump type such as a rotary lobe pump. Back pressure ~~[[5]]~~ is produced on the retentate return line 5 as desired by adjusting retentate valve 6. The transmembrane pressure during this operation can be monitored based on the pressure readings (P) 20, 21, 22 on retentate inlet 7, retentate return line 5 and permeate line 8 having pressure P. The buffer exchange solution is supplied from holding vessel 9 using pump 10 of the peristaltic or other type. During the normal operation, with the permeate in the forward direction, the permeate flow rate is monitored by flow meter 11 and controlled using control valve 12 such as a needle valve or other equivalent means for controlling flow. The permeate can be collected in waste container 13 monitoring the weight using weighing device 14 such as a scale or other equivalent apparatus. During the back pulse with the permeate in the reverse direction, the permeate flow is shut off with permeate valve 15. Inert gas valve 16 on the permeate side is opened pressurizing in-line permeate reservoir 17 at a pressure greater than the retentate pressure (P) 20, 21. This forces the permeate to flow in the reverse direction. The flow rate during the back pulse can be controlled by pressure P on inert gas ~~pressure~~ line 18 supplied from inert gas reservoir 19. After a predetermined time period or until a predetermined volume of back pulse solution has been introduced, the normal filtration process is resumed.

Please replace the paragraph beginning at page 28, line 10 with the following amended paragraph:

The setup for using saline or other aqueous solutions for the back pulse is similar to the setup used for the back pulse with permeate (Fig. 5). The setup for the actual primary filtration is the same as in Fig. 4 (items 1-[[14]] 15). However, the setup differs in the method for introducing the back pulse solution to the cross flow module. The back pulse solution is stored in vessel [[17]] 17A that is under positive pressure (P) [[18]] 23 from inert gas supply **19**. During the back pulse using an aqueous solution other than permeate, permeate valve **15** is shut off, and back pulse valve [[16]] 16A is opened. This allows the back pulse solution to flow in the reverse direction. After a predetermined time period or until a predetermined volume of back pulse solution has been introduced, the normal primary filtration process is resumed.

For the convenience of the Examiner, a clean version of the amended paragraphs as attached.